Application No. <u>10/743,624</u>
Amendment dated <u>November 30, 2007</u>
Reply to Office action dated <u>April 17, 2007</u>

Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application.

Listing of Claims:

- 1. (currently amended) A process for the oxidation of p-xylene to terephthalic acid comprising oxidizing in the liquid phase a p-xylene composition comprising at least 80 wt.% p-xylene based on the weight of liquid reactants, at a temperature in the range of 120°C to 250°C and in the presence of a solvent, a source of molecular oxygen and a catalyst composition substantially free of zirconium atoms comprising less than 5 ppm of zirconium atoms, a source of nickel (Ni) atoms, a source of manganese (Mn) atoms, and a source of bromine (Br) atoms, to form a crude reaction mixture comprising terephthalic acid and incompletely oxidized reaction products composition comprising 4-carboxybenzaldehyde (4-CBA) compounds, wherein the stoichiometric molar ratio of bromine atoms to manganese atoms is 1.5 or less, and the amount of nickel atoms is at least 500 ppm.
- 2. (original) The process of claim 1, wherein said solvent comprises an acetic acid composition.
- 3. (original) The process of claim 2, wherein said acetic acid composition comprises 2.5 to 15 wt.% water.
- 4. (original) The process of claim 1, wherein the molar ratio of Br to Ni and the molar ratio of Br to Mn are each 1.5 or less and at least 0.3.
- 5. (original) The process of claim 4, wherein the molar ratio of Br to Ni and the molar ratio of Br to Mn are each 1.1 or less.
- 6. (original) The process of claim 5, wherein the molar ratio of Br to Ni and the molar ratio of Br to Mn are each 1.0 or less.
- 7. (original) The process of claim 6, wherein the molar ratio of Br to Ni is 0.9 or less.

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- 8. (original) The process of claim 1, wherein the molar ratio of nickel atoms to manganese atoms ranges from 0.2:1 to 4:1.
- 9. (original) The process of claim 8, wherein the molar ratio of nickel atoms to manganese atoms ranges from 0.5:1 to 2.5:1.
- 10. (original) The process of claim 1, wherein the molar ratio of Br to Mn is 1.1 or less.
- 11. (original) The process of claim 10, wherein the molar ratio of Br to Mn is 1.0 or less.
- 12. (original) The process of claim 1, wherein the oxidation temperature is within a range of 140°C to 190°C and the oxidation reaction is conducted under a pressure in the range of 50 to 175 psig.
- 13. (original) The process of claim 1, wherein the catalyst composition contains less than 2 ppm Zr.
- 14. (original) The process of claim 1, wherein the catalyst composition contains less than 5 ppm cobalt.
- 15. (previously presented) The process of claim 1, wherein the reaction mixture comprises 40,000 ppm 4-CBA or less.
- 16. (original) The process of claim 1, wherein the 4-CBA content in the solids is 10,000 ppm or less.
- 17. (previously presented) The process of claim 1, wherein the ratio of solvent burn is 0.80 moles COx per mole of terephthalic acid produced or less.
- 18. (previously presented) The process of claim 17, wherein said ratio is 0.70 or less.
- 19. (original) The process of claim 1, wherein the catalyst composition is free of cobalt atoms.
- 20. (original) The process of claim 1, wherein the ratio of solvent burn is 0.60 moles COx per mole of terephthalic acid or less, and the total quantity of 4-CBA in the solid and liquid phase is 40,000 ppm or less.
- 21. (original) The process of claim 20, wherein the total quantity of 4-CBA is 10,000 ppm or less.

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Claims 22 – 28 (previously canceled).